Crysta'Days November 2023

Upscaling with the SCT-PILOT unit



The new SCT-PILOT



SCT-PILOT uses:

- Identical parameter settings as the SCT-LAB environment
- Single use fluidics for easy and complete cleaning
- All inserts and reactors are interchangeable between SCT-LAB and SCT-PILOT
- In-depth testing continuous operation and erroneous operation control
- Recipe determination
- **GLP** version available
- Government funding for independent cGMP development

Enhanced study delivers:

- Ideal coupling with maturing and isolation strategy
- Full recipe for operations with industrial equipment

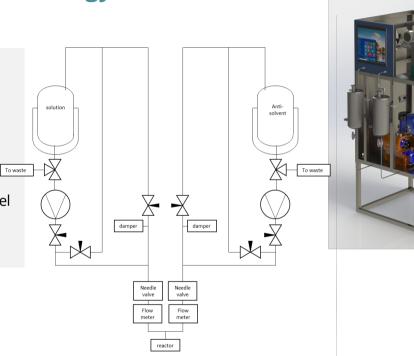
WITH LIMITED USE of TIME and material





SCT-PILOT changes in bewteen versions:

- Selection of new pump type to increase cleaning capacity and reduce material losses: 150 mL dead volume reduced to 5 mL
- Complete emptying of the vessels
- Materials in contact with chemicals:
 - Glass and PTFE
 - Interior part of pumps in stainless steel metal, other materials on request
- Identical and validated flow rate stability



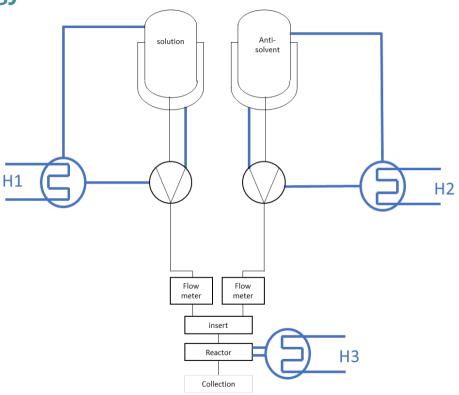






SCT-PILOT changes in bewteen versions:

- Selection of new pump type to increase cleaning capacity and reduce material losses: 150 mL dead volume reduced to 5 mL
- Complete emptying of the vessels
- Materials in contact with chemicals:
 - Glass and PTFE
 - Interior part of pumps in stainless steel metal, other materials on request
- Identical and validated flow rate stability

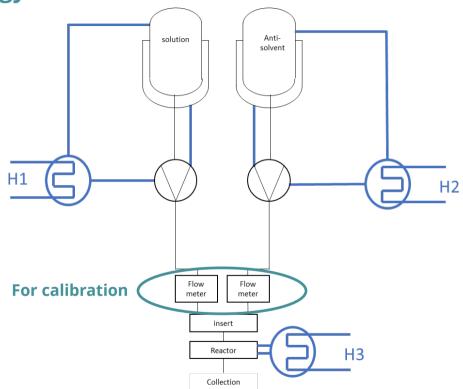






SCT-PILOT changes in bewteen versions:

- Selection of new pump type to increase cleaning capacity and reduce material losses: 150 mL dead volume reduced to 5 mL
- Complete emptying of the vessels
- Materials in contact with chemicals:
 - Glass and PTFE
 - Interior part of pumps in stainless steel metal, other materials on request
- Identical and validated flow rate stability

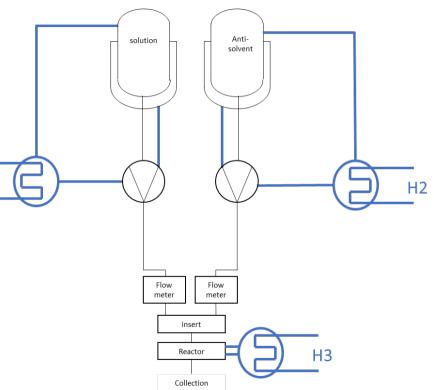






SCT-PILOT technical specifications:

- Three different temperature zones from 5 to 85°C
- Flow rates between 1 and 100 mL/min, different pump heads may lead to better stability in different ranges
- Pressure drop possible up to 40 bar very important for highly viscous materials
- Single use consumables
- Identical set of inserts and reactors
- Standard equiped with 2L glass lined vessels, agitated – may be exchanged with other vessels if required
- Pressure control for blockages
- Known OEM suppliers: Hubert thermostats and Knauer pumps.

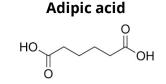


H1



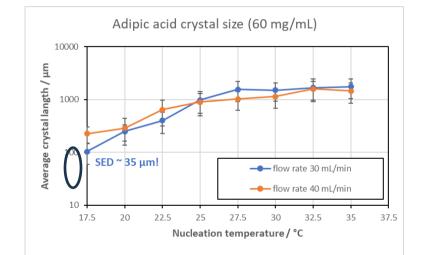






Laboratory conditions: searching for different crystal attributes

| Parameter | Adipic acid |
|--------------------------------|--------------------------------------|
| Insert | Cooling – 0 |
| Reactor | 3 mL |
| Solution temperature (°C) | 60 |
| Solution concentration (mg/mL) | 60 |
| Flow rate (mL/min) | 30 and 40 |
| Nucleation temperature °C | various |
| Crystal growth conditions | Gathering at RT, 15 minutes maturing |

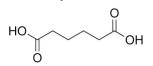


remark: lower nucleation temperatures resulted in fast blockages during cleaning



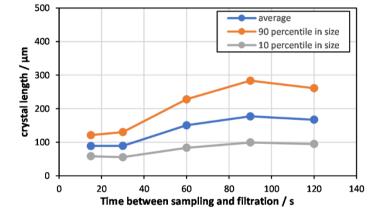
Adipic acid





Laboratory conditions: looking at crystal growth rate

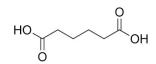
| Parameter | Adipic acid |
|--------------------------------|--|
| Insert | Cooling – 0 |
| Reactor | 3 mL |
| Solution temperature (°C) | 60 |
| Solution concentration (mg/mL) | 60 |
| Flow rate (mL/min) | 30 |
| Nucleation temperature °C | 20 |
| Crystal growth conditions | Filtration at different collection times |



remark: product gathered and filtered after one night at RT results in identical size



Adipic acid



Secoya Crystallization Technology SCT-pilot instrument long-term operation

Laboratory conditions duplicated on pilot unit: Preparation of 8 L solution

| Parameter | Adipic acid |
|--------------------------------|--------------------------------------|
| Insert | Cooling – 0 |
| Reactor | 3 mL |
| Solution temperature (°C) | 60 |
| Solution concentration (mg/mL) | 60 |
| Flow rate (mL/min) | 30 |
| Nucleation temperature °C | 17.5 |
| Crystal growth conditions | Filtration 2 minutes after gathering |

- Sampling was done every 30 minutes during 10 minutes to collect 300 mL of slurry,
- Slurry was gathered in bottle and filtered after 120 sec

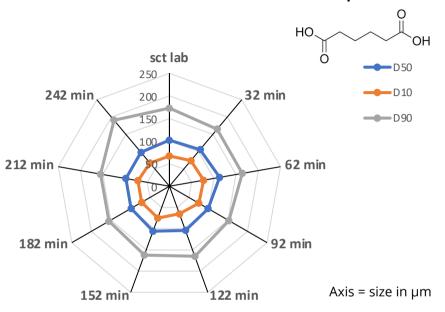


Adipic acid



Laboratory conditions duplicated on pilot unit: Preparation of 8 L solution

| Parameter | Adipic acid |
|--------------------------------|--------------------------------------|
| Insert | Cooling – 0 |
| Reactor | 3 mL |
| Solution temperature (°C) | 60 |
| Solution concentration (mg/mL) | 60 |
| Flow rate (mL/min) | 30 |
| Nucleation temperature °C | 17.5 |
| Crystal growth conditions | Filtration 2 minutes after gathering |



4 hour run without disruptions Symetry in graph indicates stability of product over time Lab parameters fully extrapolated



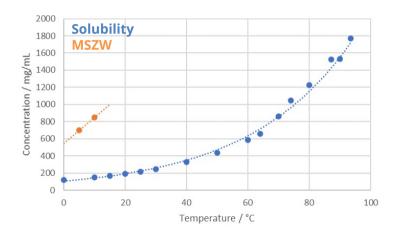




Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

remark: The insert and reactor are heavily modified to counter the viscosity effect





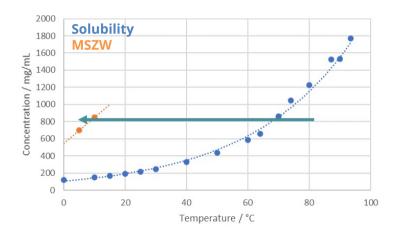




Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

remark: The insert and reactor are heavily modified to counter the viscosity effect



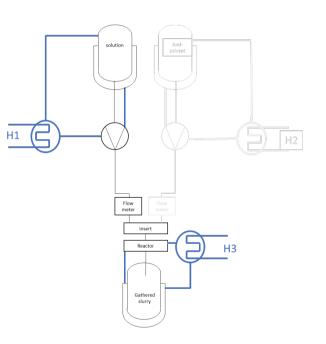




Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

remark: The insert and reactor are heavily modified to counter the viscosity effect

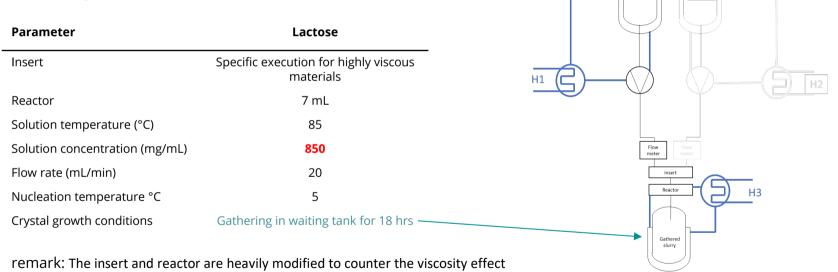




solution



Laboratory conditions set for lactose

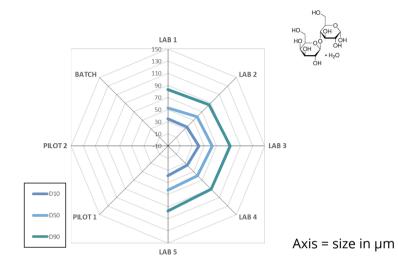




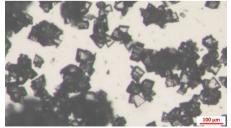


Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |



Lab repetition 1



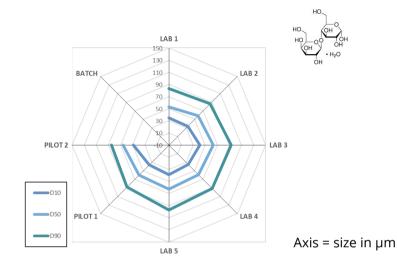




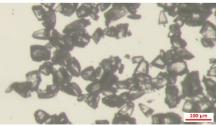
Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

2 hour run without disruptions Symmetry in graph indicates stability of product over time Lab parameters fully extrapolated



Pilot repetition 1



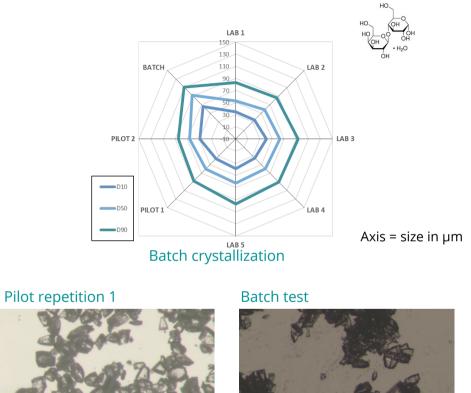




Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

Batch cross-test without passage through reactor results in 50% larger crystals with huge lumps of crystals



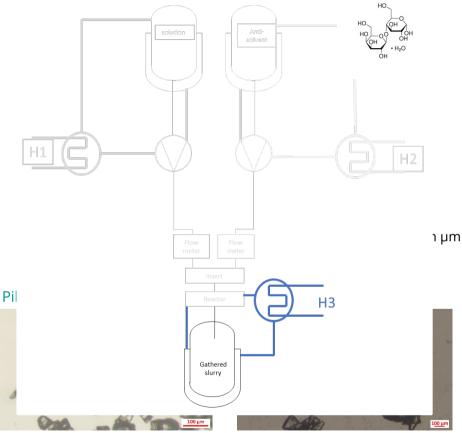




Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

Batch cross-test without passage through reactor results in 50% larger crystals with huge lumps of crystals



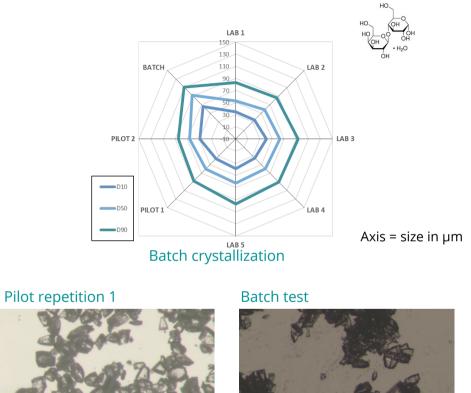




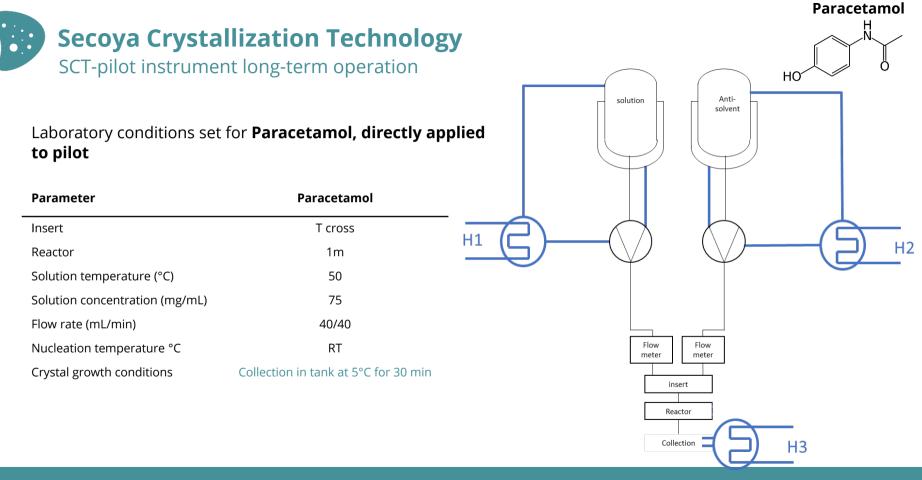
Laboratory conditions set for lactose

| Parameter | Lactose |
|--------------------------------|---|
| Insert | Specific execution for highly viscous materials |
| Reactor | 7 mL |
| Solution temperature (°C) | 85 |
| Solution concentration (mg/mL) | 850 |
| Flow rate (mL/min) | 20 |
| Nucleation temperature °C | 5 |
| Crystal growth conditions | Gathering in waiting tank for 18 hrs |

Batch cross-test without passage through reactor results in 50% larger crystals with huge lumps of crystals

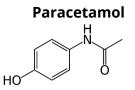






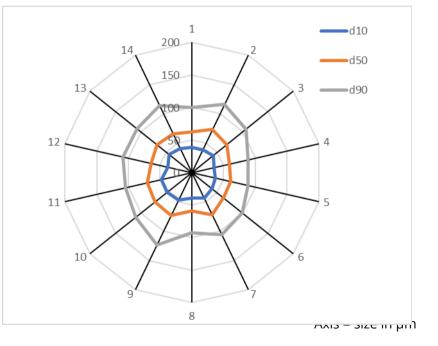






Laboratory conditions set for **Paracetamol**, **directly applied to pilot**

| Parameter | Paracetamol | | |
|--------------------------------|--------------------------------------|--|--|
| Insert | T cross | | |
| Reactor | 1m | | |
| Solution temperature (°C) | 50 | | |
| Solution concentration (mg/mL) | 75 | | |
| Flow rate (mL/min) | 40/40 | | |
| Nucleation temperature °C | RT | | |
| Crystal growth conditions | Collection in tank at 5°C for 30 min | | |





S Production strategy



INDUSTRIAL CRYSTALLIZATION UNIT – ICE is based on:

- Identical Reactor setup of laboratory equipment
- cGMP design and execution
- Molecule specific or multiproduct aproach
- Reactors in parallel in standard equipment up to 10
 modules
- Cleaning in place
- Automated software, open for communication to its surroundings
- Depending on solubilities and applied rates: 1.5 to 3 ton of solid product per module per year







INDUSTRIAL CRYSTALLIZATION UNIT – ICE is based on:

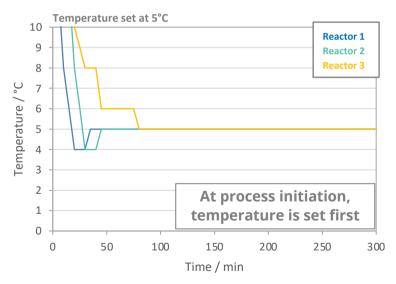
- Identical Reactor setup of laboratory equipment
- cGMP design and execution
- Molecule specific or multiproduct aproach
- Reactors in parallel in standard equipment up to 10
 modules
- Cleaning in place
- Automated software, open for communication to its surroundings
- Depending on solubilities and applied rates: 1.5 to 3 ton of solid product per module per year







Upscaling means placing **identical** reactors in **parallel** Product overall quality is defined by temperature and flow stability



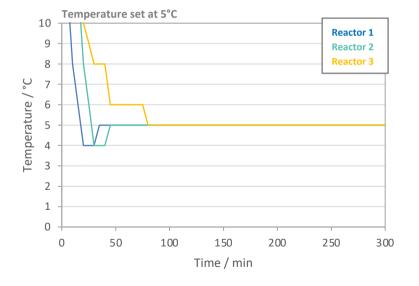


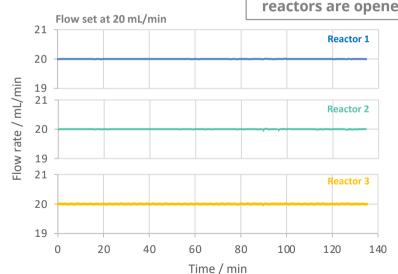


Upscaling means placing **identical** reactors in **parallel**

Product overall quality is defined by temperature and flow stability

Secondly, the reactors are opened





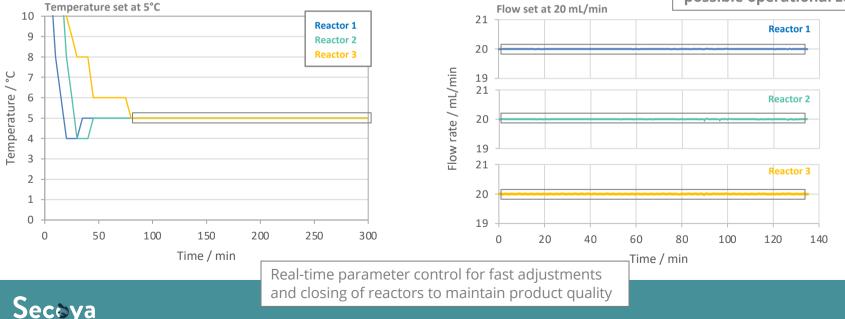




Upscaling means placing **identical** reactors in **parallel**

Product overall quality is defined by temperature and flow stability

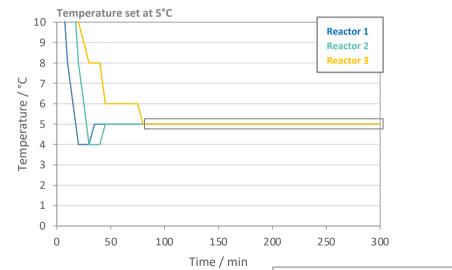
Aim for the smallest possible operational zone





Upscaling means placing **identical** reactors in **parallel**

Product overall quality is defined by temperature and flow stability



Real-time parameter control for fast adjustments and closing of reactors to maintain product quality

1. 20,05 1.

20,00 19,95 Flow set at 20 mL/min

man man



Aim for the smallest

possible operational zone

Reactor 2

Inside 0.3% deviation



Secoya Crystallization Technology

Importance of operational zonewidth

Aim:

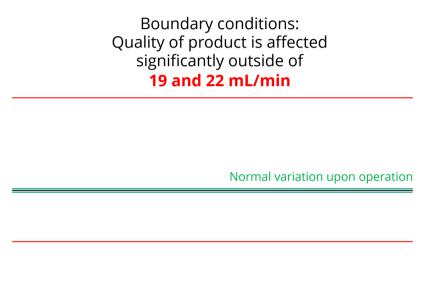
Create identical residence time at identical temperatures

Benefit:

- More uniform conditions of continuous operations means more quality control by the design of the instrument and operation
- Determination of small operational zonewidths, extra space for adjustment of tests before running out of hand

parameter

Test Flow Rate variation between 19.95 and 20.05 mL/min



Time / min





Secoya Crystallization Technology

Importance of operational zonewidth

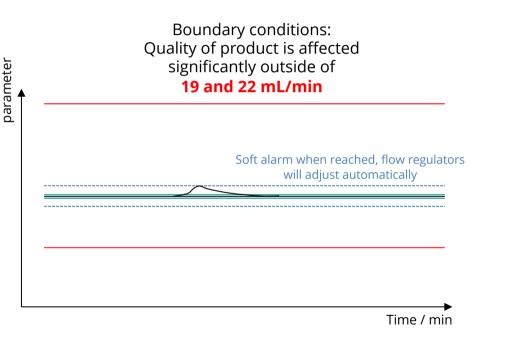
Aim:

Create identical residence time at identical temperatures

Benefit:

- More uniform conditions of continuous operations means more quality control by the design of the instrument and operation
- Determination of small operational zonewidths, extra space for adjustment of tests before running out of hand

Test Flow Rate variation between 19.95 and 20.05 mL/min







Secoya Crystallization Technology

oarameter

Importance of operational zonewidth

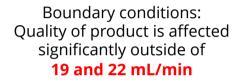
Aim:

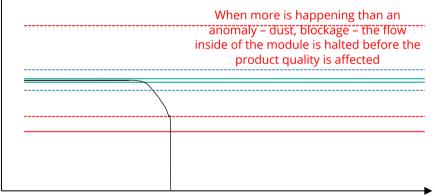
Create identical residence time at identical temperatures

Benefit:

- More uniform conditions of continuous operations means more quality control by the design of the instrument and operation
- Determination of small operational zonewidths, extra space for adjustment of tests before running out of hand

Test Flow Rate variation between 19.95 and 20.05 mL/min





Time / min



Secoya Crystallization Technology

Introduced into the parameter set on the ICE equipment





Secoya Crystallization Technology

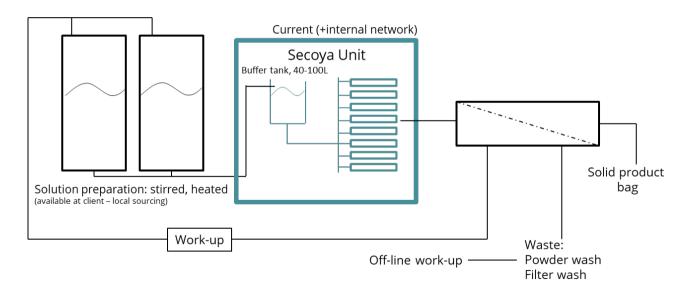
Introduced into the parameter set on the ICE equipment

| Flow rate in reactor | Module nº1 | | | Nucleation |
|----------------------|---|---|----------------------------------|-------------|
| | Setpoint flow hot circuit | Setpoint flow cold circuit | Setpoint temperature module | temperature |
| | Flow 20.0 ml/min | Flow 20.0 ml/min | Température 25.0 °C | |
| | Histérésys 5.0 ml/min | Histérésys 5.0 ml/min | Histérésys 30.0 °C | |
| | Stabilization time 17 sec | Stabilization time 15 sec | Stabilization time 15 sec | |
| | Deviation time 15 sec | Deviation time 15 sec | Deviation time 15 sec | |
| | Process value | Process value | Process value | |
| Inside modules | Flow stabilized hot circuit | Flow stabilized cold circuit | Température stabilisée | |
| | Remaining time = 0 sec | Remaining time = 0 sec | Remaining time = 0 sec | |
| | 19 20 21 18 17 22 17 | 19 20 21 18 11 2 22 17 23 16 23 16 24 15 - Echele 25 0-40ml/min 0.2 ml/min | Ethels 0 - 100 °C ##### °C | |
| | Copy setpoint for all modules Paramètres PID Mod | .1 Mod. 2 Mod. 3 Mod. 4 Mod. 5 | Number of module : 5 | |
| | | Text | | |





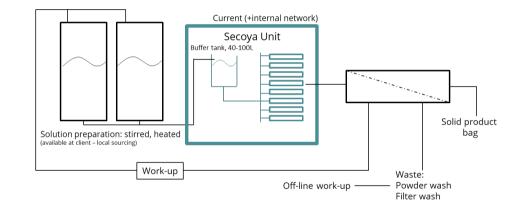
Upscaling means placing **identical** reactors in **parallel** Product overall quality is defined by temperature and flow stability







- Production request: 25 kg/day for a production of 100 kg/week
 - Only working hours, operations possible during 12 hrs: 1 hr setup, 9 hrs to run, rest for cleaning (2 shift basis with overlap)
- Solubility in solvent: 250 mg/mL
- Solubility at equilibrium (5°C): 50 mg/mL
- Possible yield: 200 mg/mL solvent
- Obtained: 94 % yield = 196 mg per mL solution injected
- Flow rate: 30 mL solution/min/reactor
- Production rate per hour ~ **350 g/hr/reactor**
- 8 reactors produce per 9 hours 25.2 kg
- Use bonus of two modules to shorten production times

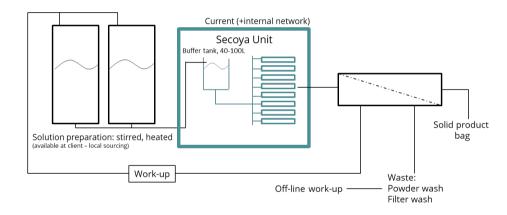


1 Growth tank to collect material at temperature, agitated Filtration with dimensionalized candle filter to shorten filtration time and to allow washing and during inside the tank with DrMueller





- Production request: **50 ton per yea**r, split in weekly productions
- 5 days' work week, cleaning procedure included, nucleation reactor may run overnight
- Solubility in solvent: 850 mg/mL
- Solubility at equilibrium (5°C): 150 mg/mL
- Possible yield: 700 mg/mL solvent
- Obtained: 95 % yield = 665 mg per mL solution injected
- Flow rate: 20 mL solution/min/reactor
- Production rate per hour ~ **798 g/hr/reactor**
- 50 reactors produce per 3 days 2.87 ton
- Ideal scenario: 17 batches per year which leaves space for events + increased production



3 growth tanks are filled consequently to cope with 18 hr growth time Filtration and CIP + module cleaning on Thursday and Friday

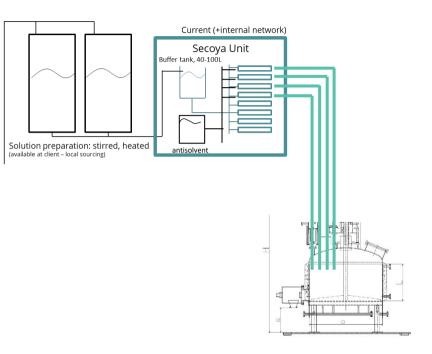




- Production request: reactive crystallization of inorganic salt
- 5 days' work week, 2 shift basis for a 12 hr production + cleaning possibility
- **5 kg solids/hour** = 200 kg/week = 9 ton/45 weeks operation
- Possible yield: 100 mg/mL solution with 1/5 mixing ratio with antisolvent

IIIII This reactive crystallization does not require a reactor, only turbulent mixing and a larger execution of the insert is applied, running at 200 mL/min for the solution side and 1000 mL/min for the antisolvent side

 4 nozzles applied, directly implemented onto a Nutsche filtration unit. Production rate attained 1.2 kg/hr/reactor







Other production strategies PIPELINE – client input



We see levels of entry that are more feasible to introduce the technology into industry:

- HPAPI: as we control the size of product and maniplations are ower
- Specific formulations: Drug product level, skipping one or more steps in DP development
- Benefit to couple to continuous tablettling machines Fette at DP level

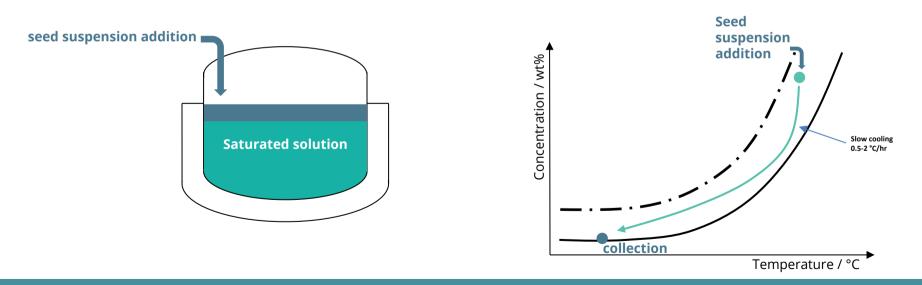
More classic API substance production, splitted from Drug product manufacturing, we see interest, but difficulties in entering into these sites as the **change** necessary to implement our units is drastic/ 'adventorous'



Preparation of high quality seeds – both dried or in suspension

Seeding Strategy

- I. Generate seeds of desired size and PSD, at equilibrium condition
- II. Add seed suspension to solution might be dried (storage) or in suspension
- III. Perform a 'classic' batch crystallization



Produced slurry used as starting point for MSMPR setup

Use as continuous feeder of nuclei into MSMPR setup

- I. Generate seeds
- II. Continuously added to first CSTR tank
- III. Product is removed from first and sent to a second at lower temperature

